Original Article

Effect of alkali treatment (NaOH) of eucalyptus leaves for hypercellulase production by *Bacillus subtilis* through submerge fermentation

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Abstract

Eucalyptus leaves were pretreated through Box-Bhenken design of response surface methodology using three variables with three levels such as NaOH concentration (0.6, 0.8, 1.0%), substrate concentration (5, 10, 15%) and residence time (4, 6, 8h) with and without steam (autoclaving at 121° C for 15min and 15psi). After pretreatment, cellulase production was conducted in 250ml Erlenmeyer flask at 50 °C, pH 5 with shaking speed of 120 rpm using 2% pretreated eucalyptus leaves as carbon source and 2% v/v inoculum size in submerged fermentation for 24h. Results showed that among these two treatments, only chemical treated substrates gave better enzyme yield as compared to chemical followed by steam. The highest FPase (2.526 IU/ml/min) activity was found at pretreatment conditions of 0.6% NaOH conc., 10% biomass loading and 4h reaction time while CMCase (2.803 IU/ml/min) at 1% NaOH conc., 15% biomass loading and 6h of reaction time. The proposed model was found highly significant as revealed by their *F*-values, *P*-values and R^2 values. Results suggest the efficiency of *Bacillus subtilis* K-18 for cellulase production from eucalyptus leaves and it would be fruitful for future industrial exploitation in all perspectives. **Keywords:** Alkali pretreatment, Eucalyptus, RSM, cellulase, *Bacillus* sp.

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INTRODUCTION

B y the recognition of the effect of fossil fuel on environment which adds to the global warming further enforce the necessity of the biofuel (McIntosh *et al.*, 2016). From the last decade research efforts increased for the second-generation biofuel production from lignocellulosic material rather than the edible crops (Pinkert *et al.*, 2009; Mussatto *et al.*, 2010; Lienqueo *et al.*, 2016). Globally the use and production of ethyl alcohol has been encouraged as biofuel is comprises of 35% oxygen which reduce the emanation of particulate matter and NO_X from fuel incineration (Ruangmee *et al.*, 2013).

The production of glucose or alcohol or biofuel or chemical initiatives from organic wastes is on its way (El-Shistawy *et al.*, 2015). Crops with the characteristics of short yield rotation, least compost contribution and quick growth while plants like pine and spruce, eucalyptus and poplar, miscanthus and switch grass from soft wood, hard wood and grasses respectively have been stipulated as preferential biofuel crops and plants species (Li *et al.*, 2015). Eucalyptus leaves are the latent auspicious cradle for biofuel production because of its cosmopolitan distribution, good growth rates and high ingathering (McIntosh *et al.*, 2016). Eucalyptus leaves are the intriguing substrate attributable to its surpassing sugar level compared to pentose sugars (Fernandes *et al.*, 2016).

Major composition of lignocellulosic biomass is cellulose, hemicellulose and lignin (Xu *et al.*, 2013). Second bountiful ingredient of lignocellulosic biomass is hemicellulose comprises of polysaccharide with diverse five and six carbon monosaccharide (Rubin 2008; Xu *et al.*, 2013) while macromolecule is lignin, possess several active sites swaying its responsiveness (Pandey and Kim, 2011;

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Norambuena et al., 2016). Lignocellulosic biomass has intractability due to more crystallinity and composite association of lignin and hemicellulose (Himmel et al., 2007; Zaho et al., 2012; Kundu et al., 2016). Pretreatment either of thermochemical technique or physiological or any-other are necessary for the fractionation of lignocellulosic biomass will promote enzymatic hydrolysis followed by saccharification for bioethanol production (Alvira et al., 2010; Akhtar et al., 2016; McIntosh et al., 2016). Cellulases are specified enzymes used for the β-1-4 glycosidic bond cleavage of glucane (Olofsson et al., 2008). Cellulases enzymes are a set of three considerable enzyme categories as endo [1-4]-B-D-glucanase, exo [1-4]- β -D-glucanase and β -D-glucosidases being designed to transform the accessible cellulosic contents to fermentable sugars (Azadian et al., 2016; Chiarello et al., 2016).

Distinct cell molders as bacteria, fungi and veasts yields cellulases which could flourish on low-cost media proven a reasonable source for the production of fermentable sugars (El-Shistawy et al., 2015). Bacterial species of Clostridium, Bacillus, Acetovibrio, Bacterioides, Microbispora, yield cellulases. Among Bacillus strains B. carboniphilus. B. sphaericus. B. subtilus, B. sp. L1 revealed the cellulytic activity (Sun and Cheng., 2002; Azadian et al., 2016). Fungi belonging to Р. Chrisosoprium, Aspergillus, Trichoderma and Shizophyllum produce cellulases. Among all these Trichoderma effectively used for cellulose production from last few decades because of its high cultivation and inducible property but it gave optimum saccharification at 50 °C (Sun and Cheng., 2002; El-Shistawy et al., 2015; Kazeem et al., 2016). Among actinomycetes C. fimi, C. uda, S. lividans, T. curvata and C. bioazotea reported for cellulolytic activity (Kuhad et al., 2011). From last three decades cellulases are commercially available and exploited equally at industrial and speculative research (Kuhad et al., 2011).

Response surface methodology is mathematical and statistical framework, useful designed for collective consequences of various variants to search the best situation for multivariable scheme (Ruangmee *et al.*, 2013; Kim *et al.*, 2016). Box- Behenken Design (BBD) for three statistic at three levels was designated (Li *et al.*, 2007; Ahmed *et al.*, 2012). Current study involves the analysis of cellulolytic activity from *Bacillus subtilis* K-18 using alkaline (NaOH) pretreated Eucalyptus leaves.

MATERIAL AND METHODS

Biomass Preparation

Eucalyptus leaves were collected from eastern garden of main library Quaid-e-Azam campus, Lahore, Punjab Pakistan, geographical coordinates are 31° 30' 15" North, 74° 18' 23" East. Collected leaves were washed to remove dust and then sundried followed by oven drying at 70 °C for overnight. The dried eucalyptus leaves were chopped and finally ground to powder form (approximately 2 mm) and used for pretreatment process.

Pretreatment Experiments

Pretreatment of eucalyptus leaves was done as described in our earlier reports (Irfan *et al.,* 2010).

Enzyme production

Enzyme production was done in 250 ml flask Erlenmever containing 25ml of fermentation medium (2% pretreated substrate and 1% yeast extract with initial medium pH 5) was autoclaved at 121°C, for 15 minutes and 15 Psi pressure. After sterilization, the flasks were allowed to cool at room temperature and 2% (v/v) of the vegetative cell culture was transferred aseptically to each of the fermentation flasks. After inoculation, the flasks were incubated at 50 °C with agitation speed of 120 rpm for 24h of fermentation period. After completion of the fermentation period, the fermented broth was filtered through muslin cloth followed by centrifugation (Sigma 2-16 PK) for 10 minutes at 10,000xg and 4°C for the removal of cell mass and unwanted particles. The clear filtrate obtained after centrifugation was used as a crude source of enzyme. Triplicate readings were taken for each of the experiment.

Analytical methods

The CMCase and FPase activities were determined as described by Arooj *et al.*, (2017).

Design of Experiment

A three variable Box-Behnken design for response surface methodology was used to study the combined effect of NaOH concentration, substrate loading and time on cellulase production over three levels. The coded and actual values of Box-Behnken design are shown in Table I. The Box-Behnken design is appropriate for examination of quadratic response surfaces and creates a second-degree polynomial model, which in turn is used in improving a process using a little number of experimental runs. Three factor Box-Behnken design with experimental as well as predicted dependent variable responses of (acid pretreatment) in which total sugar and total phenolic concentration with observed, predicted as well as residual values shown in Table II. The 13 experimental runs were randomized to exploit the effects of unsolved variability in the observed responses due to extraneous factors. The levels of the independent variables as shown in Table I were selected based on initial experiments. The relation between the coded values and actual values are described as follows:

$$x_i = \frac{X_i - X_o}{\Delta X_i}$$

Where *xi* and *Xi* are the coded and actual values of the independent variable respectively. *Xo* is the actual value of the independent variable at the center point, and ΔXi s the step change of *Xi*. A second degree polynomial was fitted to the experimental data using the statistical package software Minitab v. 17.0 to estimate the response of the dependent variable and predict the optimal point. The second degree polynomial was expressed as follows:

 $\begin{array}{l} Y{=}b_0{+}b_1X_1{+}b_2X_2{+}b_3X_3{+}b_{12}X_2{+}b_{13}X_1X_3{+}b_{23}X_2X_3{+}b_{11}X_1^2{+}b_{22}X_2^2{+}b_{33}X_3^2 \end{array}$

Where Y is predicted response, X_1 , X_2 and X_3 are independent variables, b_0 is offset term, b_1 , b_2 , b_3 are linear effects, b11, b22, b13 are interaction terms.

RESULT AND DISCUSSION

In the current study CMCase and FPase vield were analyzed from alkaline and steam alkaline pretreated eucalyptus leaves as substrate by Bacillus subtilis K-18 at 50 °C, pH 5 through submerged fermentation. Prior to enzymatic analysis eucalyptus leaves were submitted to alkaline pretreatment with NaOH concentrations (0.65, 0.8, 1%), biomass loading (5, 10, 15g) and reaction time (4, 6, 8h) and for steam alkaline pretreatment were being autoclaved at 121 °C at 15 Psi in accordance to Box Behnken design to analyze the optimal conditions for cellulase production. After pretreatment, the substrate was dried and used cellulase production in submerged for

fermentation. Experiments were conducted in triplicates and the response obtained was calculated through second order polynomial regression equations (eq 3-6). Experimental and predicted values of CMCase and FPase were mentioned in Table II and III using Box-Bhenken design. Highest FPase (2.527 IU/ml/min) production was observed in alkali treated eucalyptus leaves using pretreatment conditions 10% NaOH conc., substrate 0.6% of concentration and 4h residence time. The highest CMCase (2.803 IU/ml/min) production was noted in alkali treated eucalyptus leaves with pretreatment conditions of 1% NaOH concentration, 15% substrate concentration and 6h residence time.

Regression Equation in coded units for CMCase and FPase alkaline treated eucalyptus leaves

CMCase (IU/ml/min) =
$$8.06 - 14.59 X_1 - 0.065 X_2 + 0.039 X_3 + 5.26 X_1^2 - 0.00674 X_2^2 - 0.0607 X_3^2 + 0.2403 X_1^*X_2 + 0.581 X_1^*X_3 + 0.01400 X_2^*X_3 - 1^*X_3 + 0.01400 X_2^*X_3 - 1^*X_3 -$$

FPase (IU/ml/min) = $6.428 - 9.465 X_1 + 0.1914 X_2 - 0.5214 X_3 + 4.170 X_1^2 - 0.008365 X_2^2 + 0.00202 X_3^2 - 0.0242 X_1 + X_2 + 0.4917 X_1 + X_3 + 0.00499 X_2 + X_3 Eq. (4)$

Regression Equation in coded units for CMCase and FPase steam alkaline treated eucalyptus leaves

CMCase (IU/ml/min) = $6.894 - 8.58 X_1 - 0.0553 X_2 - 0.6547 X_3 + 3.610 X_1^2 + 0.00347 X_2^2 + 0.02761 X_3^2 + 0.0038 X_1^*X_2 + 0.3388 X_1^*X_3 + 0.00264 X_2^*X_3 Eq. (5)$

FPase (IU/ml/min) = $1.984 - 1.63X_1 + 0.2030 X_2$ - $0.141X_3 + 0.993 X_1^2 - 0.0022 X_2^2 - 0.0088 X_3^2 - 0.1814 X_1*X_2+0.2217X_1*X_3+0.0045 6 X_2*X_3 Eq. (6)$

For the assesment of significant level of second degree polynomial equation for cellulase production was performed by the implementation of analysis variance of (ANOVA). Table IV-V represents the experimental results which demonstrate the

model's effect on CMCase and FPase yeild by alkaline and steam alkaline pretreatment. For alkaline pretreatment computed Fishers F-value for CMCase was 7.15 with P-value 0.022 whereas for FPase F-value was128.54 with corresponding P-value 0.000 shows the models fitness. Model's significant level for steam alkaline pretreatment is also high-pitched as for CMCase models F-value was 29.08 with P-value 0.001 and for FPase F-value was 13.76 followed by 0.005 P-value.

Table I: Three sta	ges and series	of BBD factorial of	design of cod	ed and actual	variables
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Independent variables	Symbols	Coded and actual values		
		-1	0	+1
NaOH concentration (%)	X ₁	0.6	0.8	1
Substrate concentration (%)	X ₂	5	10	15
Time (Hours)	X ₃	4	6	8

Table II: Cellulase production by alkaline treated eucalyptus leaves using Box-Behnken design.

Run	X ₁	X ₂	X ₃	CMCase	e activity (IU/ı	ml/min)	FPase	activity (IU/	ml/min)
#				Observed	Predicted	Residual	Observed	Predicted	Residual
1	0.8	10	6	2.028056	2.028056	-0.00000	2.011852	2.011852	-0.000000
2	1.0	10	8	1.804556	2.002380	-0.19782	2.239852	2.258574	-0.018722
3	1.0	15	6	2.803241	2.634499	0.168742	2.092593	2.101741	-0.009148
4	1.0	10	4	1.790759	1.874562	-0.08380	2.087556	2.080722	0.006833
5	1.0	5	6	1.503796	1.390911	0.112885	1.824148	1.803111	0.021037
6	0.6	15	6	2.155648	2.268534	-0.11288	2.163259	2.184296	-0.021037
7	0.8	5	4	1.514833	1.543916	-0.02908	1.767111	1.794981	-0.027870
8	0.6	10	8	1.736287	1.652484	0.083803	1.892593	1.899426	-0.006833
9	0.8	15	8	1.999083	1.970001	0.029082	1.954370	1.926500	0.027870
10	0.6	10	4	2.651741	2.453917	0.197824	2.526963	2.508241	0.018722
11	0.6	5	6	1.817593	1.986334	-0.16874	1.798074	1.788926	0.009148
12	0.8	5	8	1.012028	0.927089	0.084939	1.477333	1.479648	-0.002315
13	0.8	15	4	1.941852	2.026791	-0.08493	2.044444	2.042130	0.002315

Table III: Cellulase production by steam alkaline treated eucalyptus leaves using Box-Behnken design.

Run	X ₁	X ₂	X ₃	CMCase	e activity (IU	/ml/min)	FPase	activity (IU/n	nl/min)
#				Observed	Predicted	Residual	Observed	Predicted	Residual
1	0.8	10	6	1.012648	1.012648	-0.00000	1.841778	1.841778	0.000000
2	1.0	10	8	1.151852	1.203899	-0.05204	1.704296	1.782056	-0.07775
3	1.0	15	6	1.299630	1.264663	0.034966	1.783259	1.736778	0.046481
4	1.0	10	4	1.020926	1.036545	-0.01561	1.686074	1.699833	-0.01375
5	1.0	5	6	0.960935	0.928235	0.032700	1.746963	1.701926	0.045037
6	0.6	15	6	1.518972	1.551672	-0.03270	2.264889	2.309926	-0.04503
7	0.8	5	4	1.106463	1.123544	-0.01708	1.612593	1.643870	-0.03127
8	0.6	10	8	1.243046	1.227427	0.015619	1.828889	1.815130	0.013759
9	0.8	15	8	1.365833	1.348752	0.017081	1.977630	1.946352	0.031278
10	0.6	10	4	1.654176	1.602129	0.052047	2.165333	2.087574	0.077759
11	0.6	5	6	1.195370	1.230337	-0.03496	1.503111	1.549593	-0.04648
12	0.8	5	8	0.986435	0.967088	0.019347	1.490222	1.457500	0.032722
13	0.8	15	4	1.380296	1.399643	-0.01934	1.917481	1.950204	-0.03272

Cooefficent of determination (R²) for alkaline pretreatment was 92.79% for CMCase and 99.57% for FPase stands for the same %age of the variations were well explained by the model. of these results were Validitv further authenticated by adjusted R² values which are 79.82% and 98.79% for CMCase and FPase respectively. Contingent upon steam alkaline pretreatment R² value for CMCase and FPase was 98.13 and 96.12 symbolized that 98.13%

and 96.12% variability were demonstrated by the model and only 1.87% and and 3.88% variations were credited to variables. Accuracy of R^2 was further proved by adjusted R^2 values as 94.75% and 89.13% for CMCase and FPase accordingly. In the current study thirteen experimental setups in accordance to BBD design were performed each for alkaline and steam alkaline pretreatment, here only optimal values will be discussed and compared.

Contour Plot of CMCase (IU/ml/min) vs Time, Substrate Conc. Contour Plot of CMCase (IU/ml/min) vs Time, NaOH Conc.



Contour Plot of FPase (IU/ml/min) vs Time, Substrate Conc. Contour Plot of CMCase (IU/ml/min) vs Substrate Conc., NaOH Conc.



Contour Plot of FPase (IU/ml/min) vs Time, NaOH Conc. Contour Plot of FPase (IU/ml/min) vs Substrate Conc., NaOH Conc.



Figure 1. FPase and CMCase production from alkaline treated eucalyptus leaves

Abou-Taleb et al. (2009) reported CMCase 2.39U/ml and 1.18U/ml FPase activity carboxymethyl cellulase from using В. amyloliquefaciens C2. Sethi et al. (2013) reported CMCase production was 0.9U/ml from coconut cake by using Bacillus subtilis at 49 °C lesser than the current study. Number of carbon sources were used for fermentation, posed a great impact on cellulase production. B. licheniformis 2D55 3% v/v hydrolyzed alkaline pretreated sugarcane bagasse and rice husk with 29.4U/ml CMCase and 12.9U/ml FPase activity at 60 °C with 18h fermentation (Kazeem et al., 2016). While alkaline pretreated rice straw hydrolyzed by Trichoderma virens produced

lower CMCase (1669.65U/g) and FPase (93.75U/ml) (Rahnama et al., 2014). Badhan et al., (2007) produced 6.62U/g CMCase and 0.7U/g FPase from Myceliophthora SD. IMI387099 using bagasse as a carbon source. In the present study alkaline (NaOH) pretreated eucalyptus leaves peaked CMCase and FPase activities was 2.803IU/ml/min and 2.526IU/ml/min accordingly at pH-5, 50 °C for 24h of fermentation by Bacillus subtilis K-18. While for steam alkaline steam pretreated eucalyptus leaves under the same fermentation conditions uppermost observed CMCase and FPase activities were 1.6544IU/ml/min and 2.264IU/ml/min respectively.

Fable IV: ANOVA for cellulase fron	alkaline pretreated	Eucalyptus leaves
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CMCase	Sources	DF	Adj SS	Adj MS	F value	P value
(IU/ml/min)	Model	9	2.45803	0.27311	7.15	0.022
	Linear	3	1.41722	0.47241	12.38	0.009
	X ₁	1	0.02633	0.02633	0.69	0.444
	X ₂	1	1.16401	0.16401	30.49	0.003
	X ₃	1	0.22688	0.22688	5.94	0.059
	Square	3	0.51546	0.17182	4.50	0.069
	X_1^2	1	0.16353	0.16353	4.28	0.093
	X_{2}^{2}	1	0.10475	0.10475	2.74	0.159
	X_{3}^{2}	1	0.21744	0.21744	5.70	0.063
	2 Way interaction	3	0.52535	0.17512	4.59	0.067
	$X_1 X_2$	1	0.23107	0.23107	6.05	0.057
	X ₁ *X ₃	1	0.21588	0.21588	5.66	0.663
	$X_2 X_3$	1	0.07841	0.07841	2.05	0.211
	Error	5	0.19087	0.03817		
	Lack of fit	3	0.19087	0.06362		
	Pure error	2	0.00000	0.00000		
	Total	14	2.64890			
EDeee	Courses	DE	74! 66	A di Me	Evalue	D value
rrase	Sources	DF	Auj 33	AUJ WIS	i value	F value
(IU/ml/min)	Model	9	0.789215	0.087691	128.54	0.000
(IU/ml/min)	Model Linear	9 3	0.789215 0.336020	0.087691	128.54 164.18	0.000 0.000
(IU/ml/min)	Model Linear X ₁	9 3 1	0.789215 0.336020 0.002337	0.087691 0.112007 0.002337	128.54 164.18 3.43	0.000 0.000 0.123
(IU/ml/min)	Model Linear X ₁ X ₂	9 3 1 1	0.789215 0.336020 0.002337 0.240818	0.087691 0.112007 0.002337 0.240818	128.54 164.18 3.43 352.99	0.000 0.000 0.123 0.000
(IU/ml/min)	Model Linear X ₁ X ₂ X ₃	9 3 1 1 1	0.789215 0.336020 0.002337 0.240818 0.092865	0.087691 0.112007 0.002337 0.240818 0.092865	128.54 164.18 3.43 352.99 136.12	0.000 0.000 0.123 0.000 0.000
(IU/ml/min)	Model Linear X ₁ X ₂ X ₃ Square	9 3 1 1 1 3	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391	128.54 164.18 3.43 352.99 136.12 139.82	0.000 0.000 0.123 0.000 0.000 0.000
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square $X_{1_2}^2$	9 3 1 1 1 3 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724	128.54 164.18 3.43 352.99 136.12 139.82 150.57	0.000 0.000 0.123 0.000 0.000 0.000 0.000
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2	9 3 1 1 1 3 1 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.000
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2	9 3 1 1 3 1 1 1 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.000 0.578
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction	9 3 1 1 3 1 1 1 3	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$	9 3 1 1 3 1 1 3 1 3 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$	9 3 1 1 3 1 1 3 1 3 1 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340 0.154711	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340 0.154711	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43 226.77	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123 0.000
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$	9 3 1 1 3 1 1 3 1 1 3 1 1	0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340 0.154711 0.009970	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340 0.154711 0.009970	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43 226.77 14.61	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123 0.000 0.12
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ Error	9 3 1 1 3 1 1 3 1 1 3 1 5	Auj 33 0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340 0.154711 0.009970 0.003411	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340 0.154711 0.009970 0.000682	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43 226.77 14.61	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123 0.000 0.12
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ ErrorLack of fit	9 3 1 1 3 1 1 3 1 1 3 1 5 3	Auj 33 0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340 0.154711 0.009970 0.003411	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340 0.154711 0.009970 0.000682 0.001137	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43 226.77 14.61	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123 0.000 0.12
(IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ ErrorLack of fitPure error	9 3 1 1 3 1 1 3 1 1 5 3 2	Auj 33 0.789215 0.336020 0.002337 0.240818 0.092865 0.286174 0.102724 0.161484 0.000242 0.167021 0.002340 0.154711 0.003411 0.003411 0.00000	0.087691 0.112007 0.002337 0.240818 0.092865 0.095391 0.102724 0.161484 0.000242 0.55674 0.002340 0.154711 0.009970 0.000682 0.001137 0.000000	128.54 164.18 3.43 352.99 136.12 139.82 150.57 236.70 0.35 81.61 3.43 226.77 14.61	0.000 0.000 0.123 0.000 0.000 0.000 0.000 0.000 0.578 0.000 0.123 0.000 0.12



Contour Plot of CMCase (IU/ml/min) vs Time, Substrate Conc. Contour Plot of CMCase (IU/ml/min) vs Time, NaOH Conc.









Figure 2: FPase and CMCase production from steam alkaline pretreated eucalyptus leaves

CMCase	Sources	DF	Adj SS	Adj MS	F value	P value
(IU/ml/min)	Model	9	0.618797	0.068755	29.08	0.001
	Linear	3	0.411349	0.137116	57.99	0.000
	X ₁	1	0.173526	0.173526	73.39	0.000
	X ₂	1	0.216327	0.216327	91.49	0.000
	X ₃	1	0.021496	0.021496	9.06	0.030
	Square	3	0.131149	0.043716	18.49	0.004
	$X_{1_{2}}^{2}$	1	0.077001	0.077001	32.57	0.002
	X_{2}^{2}	1	0.027734	0.027734	11.73	0.019
	X_{3}^{2}	1	0.045036	0.045036	19.05	0.007
	2 Way interaction	3	0.076299	0.025433	10.76	0.013
	X ₁ *X ₂	1	0.000057	0.000057	0.02	0.883
	X ₁ *X ₃	1	0.073456	0.073456	31.07	0.003
	$X_{2}^{*}X_{3}$	1	0.002786	0.002786	1.18	0.327
	Error	5	0.011822	0.002364		
	Lack of fit	3	0.011822	0.003941		
	Pure error	2	0.000000	0.000000		
	Total	14	0.630619			
FPase	Sources	DF	Adj SS	Adj MS	F value	P value
FPase (IU/ml/min)	Sources Model	DF 9	Adj SS 0.617695	Adj MS 0.068633	F value 13.76	P value 0.005
FPase (IU/ml/min)	Sources Model Linear	DF 9 3	Adj SS 0.617695 0.422795	Adj MS 0.068633 0.140932	F value 13.76 28.25	P value 0.005 0.001
FPase (IU/ml/min)	Sources Model Linear X ₁	DF 9 3 1	Adj SS 0.617695 0.422795 0.088543	Adj MS 0.068633 0.140932 0.088543	F value 13.76 28.25 17.75	P value 0.005 0.001 0.008
FPase (IU/ml/min)	Sources Model Linear X ₁ X ₂	DF 9 3 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160	Adj MS 0.068633 0.140932 0.088543 0.316160	F value 13.76 28.25 17.75 63.37	P value 0.005 0.001 0.008 0.001
FPase (IU/ml/min)	Sources Model Linear X ₁ X ₂ X ₃	DF 9 3 1 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092	F value 13.76 28.25 17.75 63.37 3.63	P value 0.005 0.001 0.008 0.001 0.115
FPase (IU/ml/min)	Sources Model Linear X ₁ X ₂ X ₃ Square	DF 9 3 1 1 1 3	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848	F value 13.76 28.25 17.75 63.37 3.63 1.57	P value 0.005 0.001 0.008 0.001 0.115 0.306
FPase (IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square $X_{1_2}^2$	DF 9 3 1 1 1 3 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329
FPase (IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2	DF 9 3 1 1 1 3 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182
FPase (IU/ml/min)	SourcesModelLinear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2	DF 9 3 1 1 3 1 1 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_2^2 X_3^2 2 way interaction	DF 9 3 1 1 3 1 1 1 3 3	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$	DF 9 3 1 1 3 1 1 3 1 3 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$	DF 9 3 1 1 3 1 1 3 1 3 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581 0.031447	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581 0.031447	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37 6.30	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004 0.054
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$	DF 9 3 1 1 3 1 1 3 1 1 3 1 1	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581 0.031447 0.008328	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581 0.031447 0.008328	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37 6.30 1.67	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004 0.054 0.253
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ Error	DF 9 3 1 1 3 1 1 3 1 1 5	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581 0.031447 0.008328 0.025947	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581 0.031447 0.008328 0.004989	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37 6.30 1.67	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004 0.054 0.253
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ Error Lack of fit	DF 9 3 1 1 3 1 1 3 1 1 5 3	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581 0.031447 0.008328 0.025947 0.024947	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581 0.031447 0.008328 0.004989 0.008316	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37 6.30 1.67	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004 0.054 0.253
FPase (IU/ml/min)	Sources Model Linear X_1 X_2 X_3 Square X_1^2 X_2^2 X_3^2 2 way interaction $X_1^*X_2$ $X_1^*X_3$ $X_2^*X_3$ Error Lack of fit Pure error	DF 9 3 1 1 3 1 1 3 1 1 5 3 2	Adj SS 0.617695 0.422795 0.088543 0.316160 0.018092 0.023544 0.005826 0.011973 0.004614 0.171356 0.131581 0.031447 0.008328 0.025947 0.024947 0.000000	Adj MS 0.068633 0.140932 0.088543 0.316160 0.018092 0.007848 0.005826 0.011973 0.004614 0.057119 0.131581 0.031447 0.008328 0.004989 0.008316 0.00000	F value 13.76 28.25 17.75 63.37 3.63 1.57 1.17 2.40 0.92 11.45 26.37 6.30 1.67	P value 0.005 0.001 0.008 0.001 0.115 0.306 0.329 0.182 0.380 0.011 0.004 0.054 0.253

Table V: ANOVA for cellulase from steam alkaline pretreated Eucalyptus leaves

Figure 1 and 2 presented contour plots for cellulase production by Bacillus subtilis K-18 submerged fermentation using in alkali pretreated and alkali steam pretreated eucalyptus leaves. These plots clearly explained the significance of individual parameter of pretreatment on cellulase production. Vyas et al. (2016) stated that Bacillus subtilis M1 produced high titer of exoglucanase and endoglucanase by alkali treated ground nut shell as compared to and untreated substrate. Mahalakshmi Jayalakshmi (2016) described that alkali treated sugarcane bagasse yield better cellulase production from Achromobacter xylosoxidans. Assareh et al., (2012) produced 143.50U/ml CMCase from Geobacillus sp. T1 AT 50 °C using barely straw as substrate. Asha and

Sakthivel (2014) reported 22.9U/ml CMCase activity from *Bacillus subtilis* using carboxymethyl cellulase (CMC) as substrate being lower than current study.

Conclusion

Results of this study indicated that alkali pretreatment of the eucalyptus leaves favored hyper cellulase production by *Bacillus subtilis* K-18 in submerged fermentation at 50°C for 24h of fermentation period. The cellulase enzyme produced from this strain could be used in various industrial sectors especially in biofuels.

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